



Towards resource recovery from industrial wastewater treatment by tubing two-phase partitioning bioreactors: challenges and perspectives

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OUTLINE

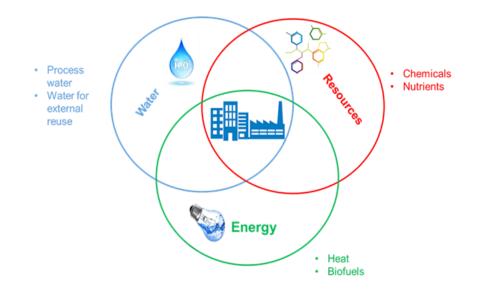


- Introduction: biological treatment of industrial wastewater and resource recovery
- Objectives
- Technology: Solid-liquid Two-phase Partitioning Bioreactors (TPPBs)
 - Granular-Polymer TPPBs
 - Tubing TPBBs
- Experimental
- Results and discussion
- Conclusions and future developments

INTRODUCTION



Energy and resource recovery concept in industry







Effluent composition :

- diverse types of pollutants including additives, solvents, biocides, and other toxic organic compounds potentially biodegradable but often difficult to biodegrade (usually at high concentrations)
- inorganic components (i.e. tanning agents, heavy metals, salts), which would normally be incompatible for biological treatment causing a "hostile" reaction environment



To demonstrate the feasibility of the tubing-TPPB system for treating industrial wastewater

Effective removal of the organic load

Complete separation for recovery (when suitable) of inorganics

Granular

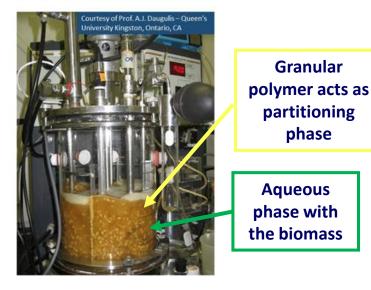
partitioning

phase

Aqueous



Solid-liquid TPPB: principle of operation



- Addition of polymer beads to a conventional bioreactor
- Substrate partitions between polymer and liquid phase
- Release of substrates into liquid phase, where biodegradation occurs

Features

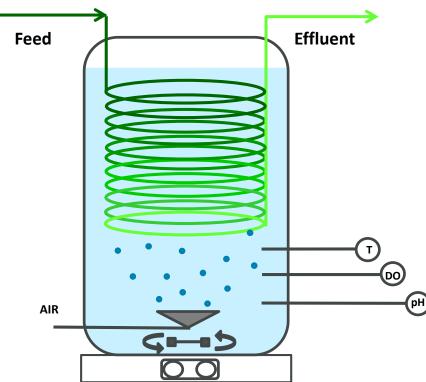


- Self-regulating system (based on metabolic processes)
- Effective in presence of high xenobiotic concentration for biomass inhibition control
- > Application to industrial wastewater treatment (more advantageous in sequential systems)

TUBING-TPPB

Tubing-TPPB: principle of operation

Configuration of an Extractive Membrane Bioreactor (Livingston et al., 1998) operated with polymeric (instead of silicon rubber) tubing suitable for a wider spectrum of organics



- A coiled polymeric tubing is immersed in the bioreactor
- Wastewater flows inside tubing
- Organic substrate diffuses across tubing walls towards bioreactor liquid side
- Biodegradation occurs in the bulk phase containing the biomass



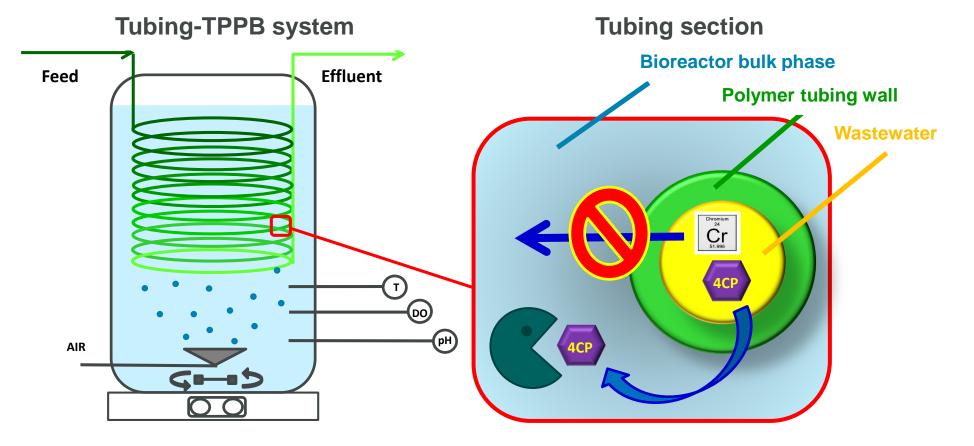
Livingston A.G. et al. (1998) J. Membr. Sci. 151, 29-44.



TUBING-TPPB

Features

- > Selective transfer and **removal** of organics and **simultaneous separation for recovery** of inorganics
- Separation of the biomass from the wastewater is advantageous for the application to «hostile» industrial wastewater
- Continuous operation (C-TPPB)

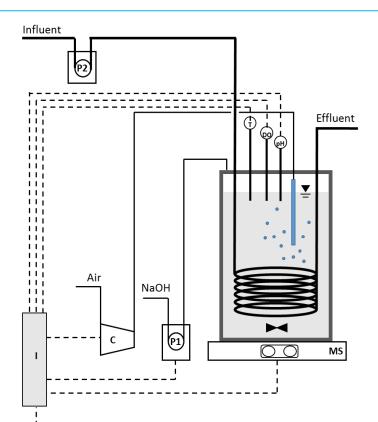






EXPERIMENTAL

Tubing made of Hytrel (DuPont, Canada)		
Lenght	3.5-5.5	m
Internal volume	0.1	L
Internal flow rate	0.02-0.06	L/h
Tubing-TPPB bioreactor		
Volume	4	L
Temperature	27	°C
рН	7.5	-
Dissolved Oxygen (DO)	3-4	mg/L
Tannery wastewater (TW)		
4-chlorophenol (4CP)	1-2.5	g/L
Potassium Dichromate (as CrVI)	100	mg/L
Saline wastewater (SW)		
2,4-dimethylphenol (DMP)	1.2	g/L
Sodium Chloride (NaCl)	100	g/L



Tubing selection

РС

Hytrel 8206 and Hytrel G3548 were selected for tannery and saline wastewatwer respectively, according to previous results on the use of this material in granular form.

Tomei et al., J. Environ. Manag. (2015) 150, 81–91; Tomei et al., Sci.Tot. Env. (2017), 500-600, 1056-1063.



EXPERIMENTAL

Abiotic tests

Mass transfer tests (continuous feed for 24 h)

> Biotic tests

Biodegradation tests (*continuos feed with increasig step loading conditions*) by using a mixed culture already acclimatized to 4CP/DMP to inoculate the tubing-TPPB system

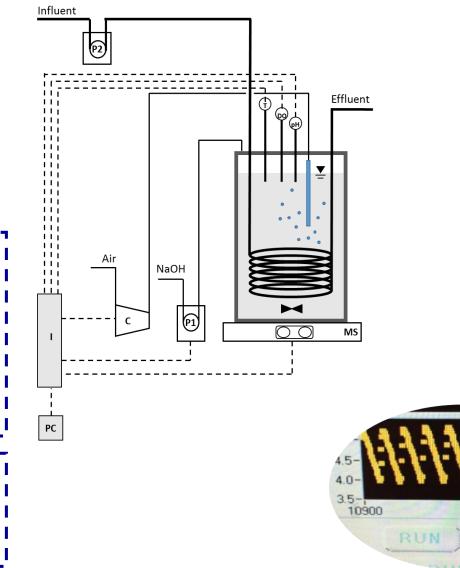
Analysis of 4CP and CrVI (TW) Analysis of DMP andl Cl⁻ (SW)

- Bioreactor
- Tubing effluent
- Collected effluent

To evaluate mass balance

On-off control of DO, i.e. on line evaluation of the Specific Oxygen Uptake Rate (SOUR)

To evaluate metabolic activity

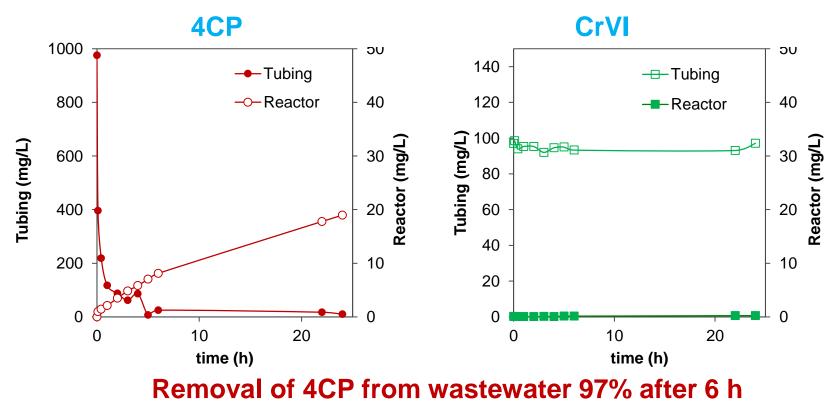




RESULTS AND DISCUSSION - TANNERY

Abiotic test for mass transfer study

MT_TW Influent : 4CP = 1000 mg/L CrVI = 100 mg/L



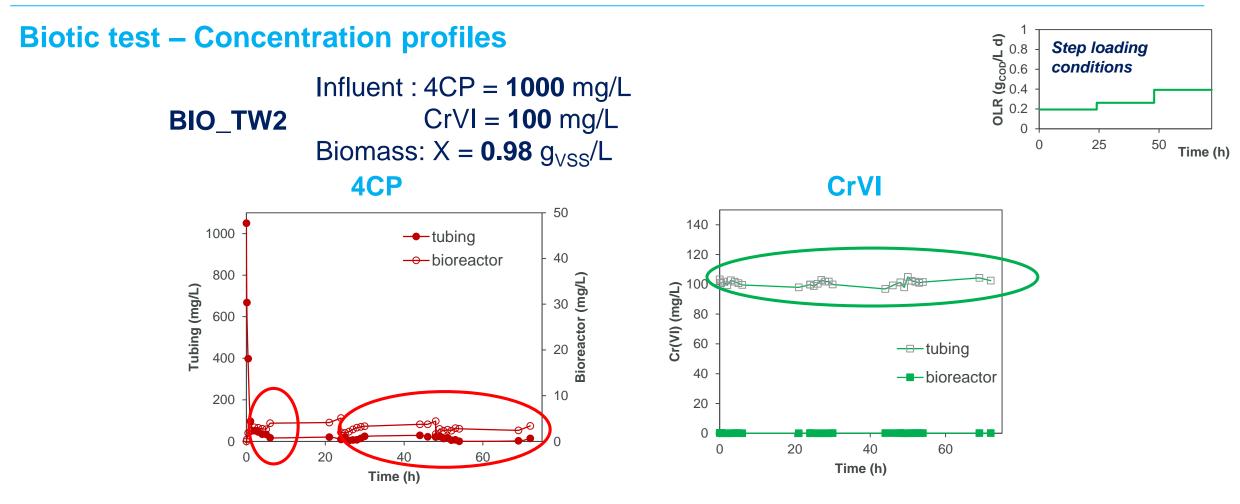
No transfer of CrVI through the polymer tubing



Hytrel 8260

RESULTS AND DISCUSSION - TANNERY





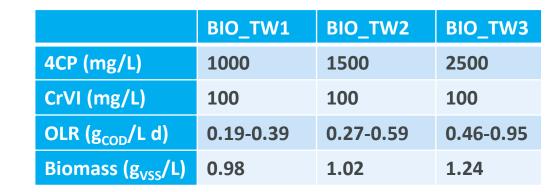
Removal of 4CP from wastewater 98% after 5 h and 99% from 24 to 72 h

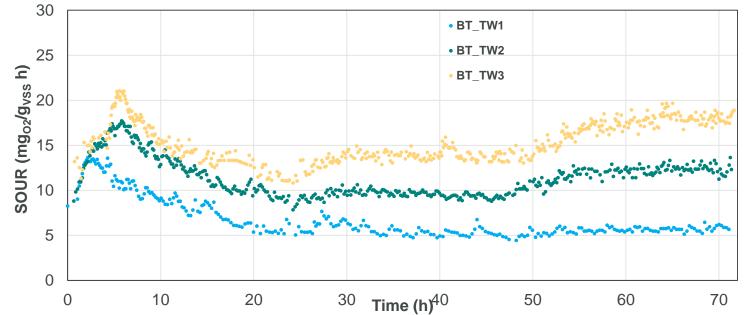
Complete recovery of CrVI in the tubing effluent

RESULTS AND DISCUSSION - TANNERY



Biotic test – SOUR

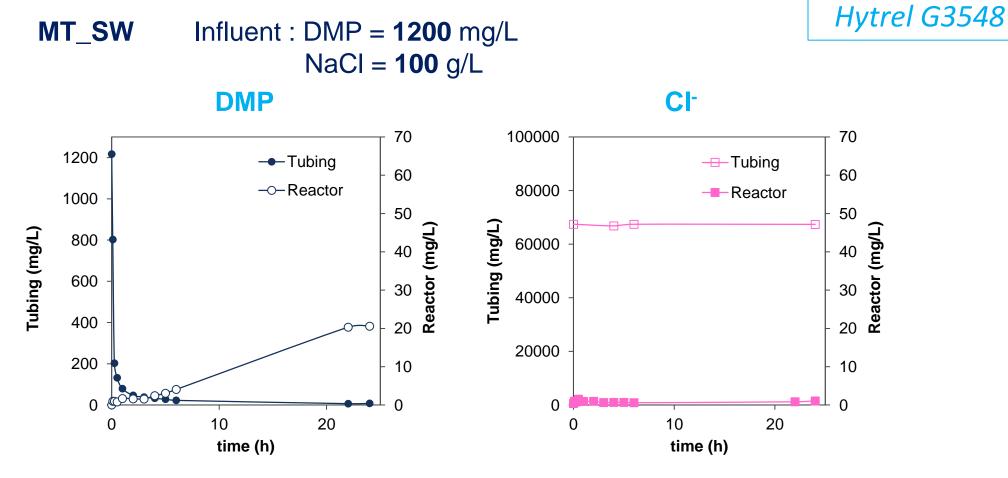




In spite of the increased influent concentration, it was observed no inhibition and enhanced microbial activity



Abiotic test for mass transfer study



Removal of DMP from wastewater 98% after 6 h

No transfer of NaCl through the polymer tubing

RESULTS AND DISCUSSION - SALINE

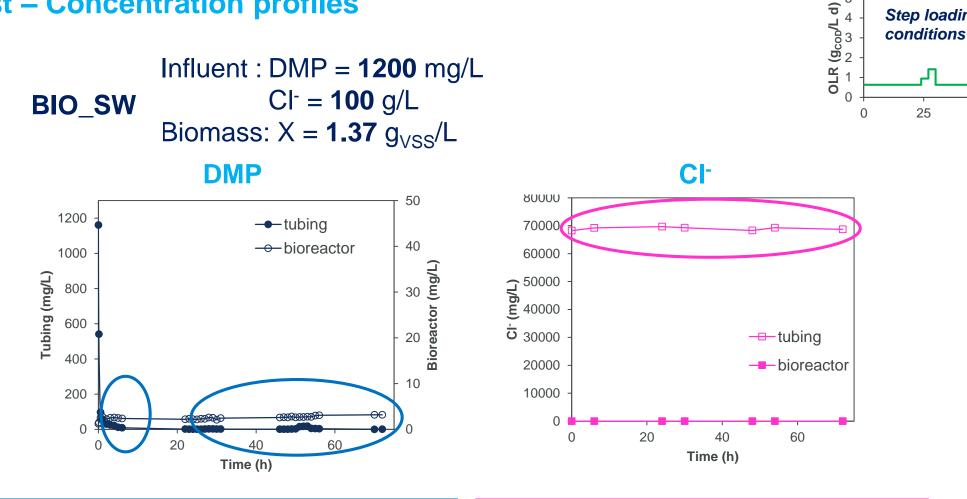


Time (h)

Step loading

50

Biotic test – Concentration profiles



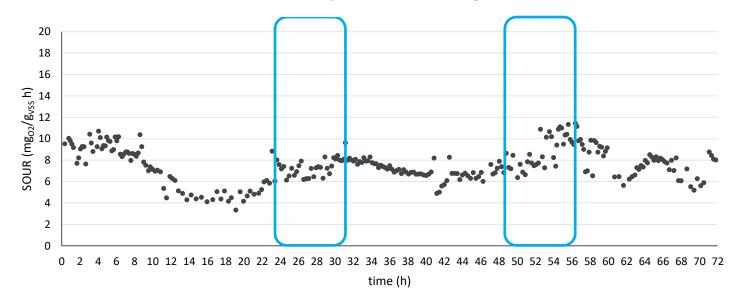
Removal of DMP from wastewater 99% after 5 h and until 72 h

Complete recovery of NaCl in the tubing effluent

RESULTS AND DISCUSSION - SALINE



Biotic test – SOUR



Step increasing loads

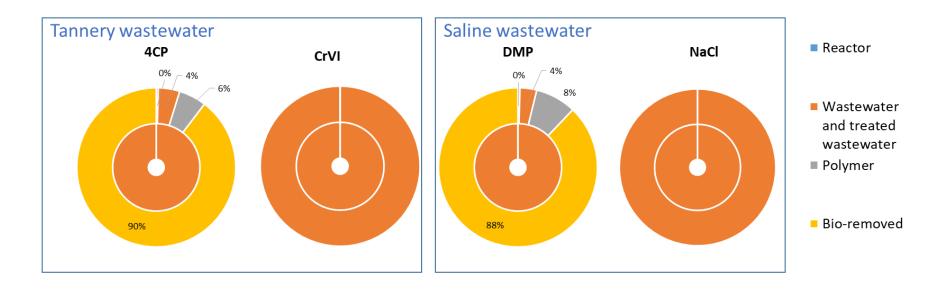
In spite of the increased influent flow rate, it was observed no inhibition and enhanced microbial activity

RESULTS AND DISCUSSION



Biotic test – Mass balance

Overview of distribution of investigated compounds during BT tests. (Inner circle is for t=0 and outer circle is for t=72 h)



- Biodegradation efficiencies were within the range of 88-90%
- The fraction retained by the polymer itself has been always <9% of the fed amount, so demonstrating that the effective degradation of the organics transferred across the polymer walls and not only the sorption took place



- The proposed hybrid bioreactor has significant potential in treating "hostile" industrial wastewater
- Biodegradation of toxic organic molecules was successfully achieved and the microbial activity was not affected by the influent wastewater composition and concentration
- > The hybrid bioreactor achieved the complete recoverable inorganic separation
- The high quality level of the effluent would allow the water reuse in the production cycle and/or the recovery of valuable resources

The demonstrated advantages of tubing-TPPB system fall within the basic principles of "*reduce, reuse and recycle*" required by a cleaner and eco-efficient improved production.



Optimization of operating parameters to control the process performance

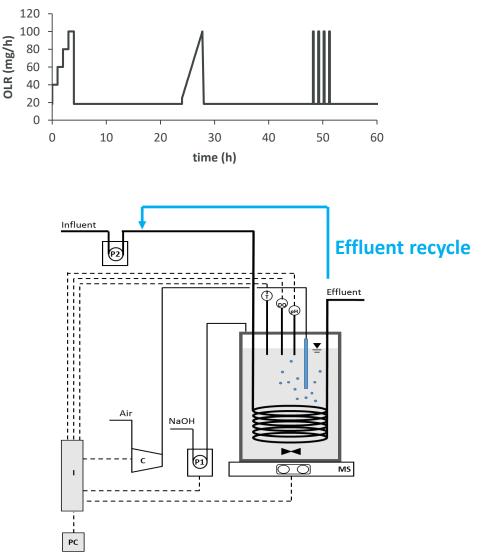
Long-term operation

Analysis of the process performance and polymer self-regeneration for times of the order of months

Effluent recycle application

Analysis of the system performance at different recycle ratios to verify the potential mitigation effect of the effluent recycle with increasing loadings

Test on real industrial wastewater Verification of the hybrid technology





- Tomei M.C., Mosca Angelucci D. (2019). Enhancing biodegradation of toxic industrial wastewater in a continuous two-phase partitioning bioreactor operated with effluent recycle. Process Safety and Environmental Protection 124, 172-180.
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- Tomei M.C. Mosca Angelucci D., Stazi V., Daugulis A.J. (2017). On the applicability of a hybrid bioreactor operated with polymeric tubing for the biological treatment of saline wastewater. Science of the Total Environment, 599-600, 1056-1063.
- Mosca Angelucci D., Stazi V., Daugulis A.J., Tomei M.C. (2017). Treatment of synthetic tannery wastewater in a continuous two-phase partitioning bioreactor: biodegradation of the organic fraction and chromium separation. Journal of Cleaner Production, 152, 321-329.
- Tomei M.C., Mosca Angelucci D., Daugulis A.J. (2017). A novel continuous two-phase partitioning bioreactor operated with polymeric tubing: performance validation for enhanced biological removal of toxic substrates. Journal of Environmental Management, 187, 265-272.
- Tomei M.C. Mosca Angelucci D., Daugulis A.J. (2016). Towards a continuous two-phase partitioning bioreactor for xenobiotic removal. Journal of Hazardous Materials, 317, 403–415.



IWA-IDB INNOVATION CONFERENCE ON SUSTAINABLE USE OF WATER: Cities, Industry and Agriculture



Thanks for the attention

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